

# LEVERAGING CAPE-OPEN FOR ENHANCED MULTIPHASE PUMP DESIGN AND PROCESS SIMULATION

CAPE-OPEN 2025 ANNUAL MEETING

GHENT – BELGIUM

V. CARIES, M. GAINVILLE, V. MOENNE-LOCCOZ

# PRESENTATION BREAKDOWN

1. **IFPEN role in CAPE-OPEN:** past contributions & motivations for the current work
2. **Multiphase pump software:** leveraging CAPE-OPEN Python Unit Operation
3. **Conclusions & perspectives**

# INTRODUCTION

# IFPEN INVOLVEMENT IN CAPE-OPEN ACTIVITIES

## Key roles

- Managed CAPE-OPEN and Global CAPE-OPEN projects (1997-2002)
- Co-founded CO-LaN and contributed actively (2001–2011)
- Transitioned to corporate associate member in 2011

## Contributions & applications

- Developed a wizard for Unit Operation (UO) in C++
- Developed UO (e.g., Hysipipe for hydrate transportability, Desulfo+ for gas sweetening)
- Introduced CAPE-OPEN support to Carnot, our in-house thermodynamic server
- Extensive use of CAPE-OPEN-supporting tools like COFE, Multiflash®, PRO/II™, HYSYS®...

# OVERVIEW OF MULTIPHASE PUMP (MPP) ACTIVITIES

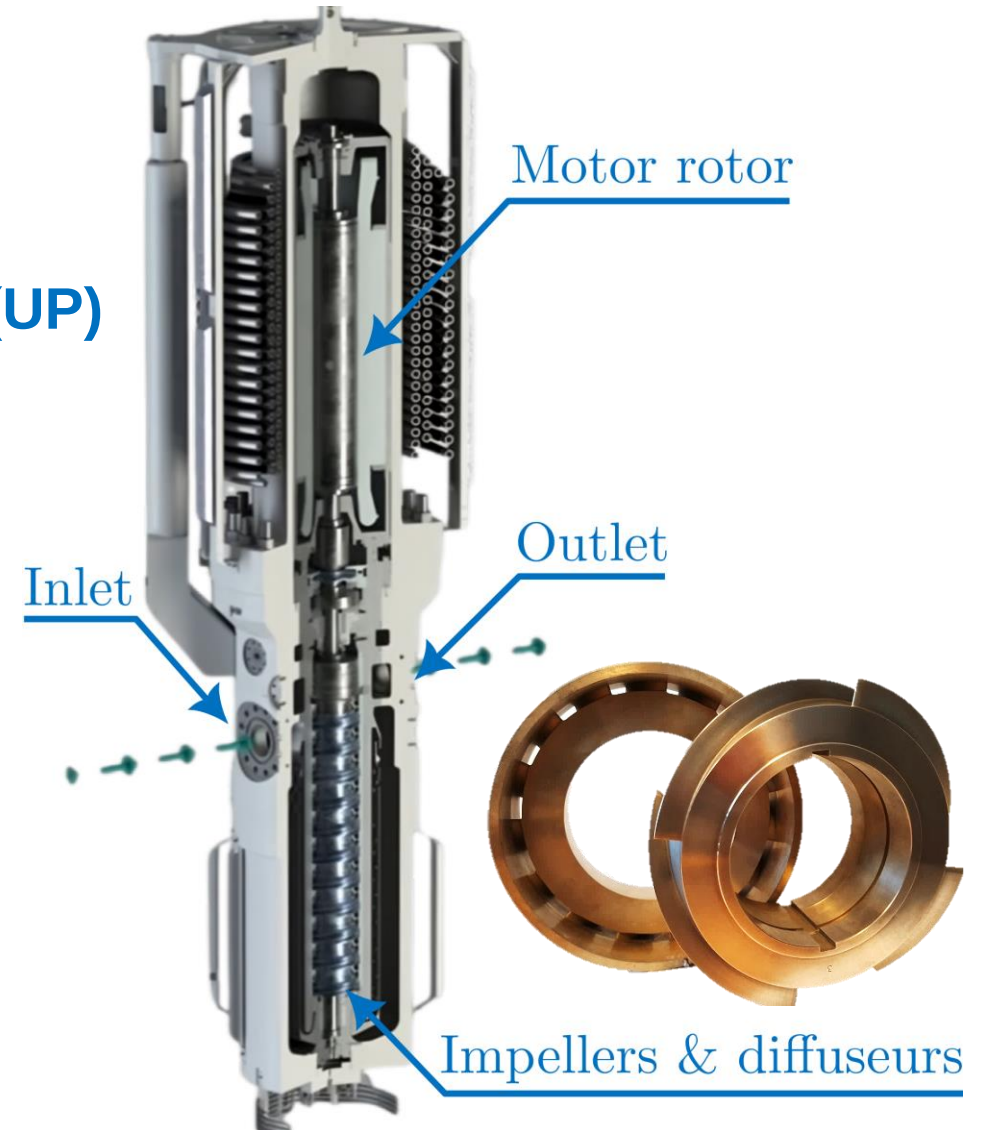
**Over 40 years of expertise in MPP design**

**Historical applications in upstream petroleum (UP)**

- Wellhead pumps: 100+ units
- Downhole pumps: 1,000+ units

**MPP key features**

- Gas volume fraction: up to 90%
- Flow rate: up to 400 m<sup>3</sup>/h
- Pressure increase: up to 200 bar



Source: SLB OneSubsea

# MOTIVATIONS

## Outputs from past UP activities

- Proprietary software for MPP design, performance, and selection
- Proven MPP robustness and reliability derived from extensive UP experience

## Leverage MPP potential by expanding its application range

- Lower CAPEX: equipment replacement synergy → compressor + pump = single MPP
- Lower OPEX: maintenance cost reduction & lower downtime

## Current needs: evaluation and optimization of MPP integration into new processes

- Embedding proprietary MPP design code into PME (Process Modeling Environments)
- AmsterCHEM CAPE-OPEN Python UO identified as an ideal framework

# LEVERAGING AMSTERCHEM CAPE-OPEN PYTHON UNIT OPERATION

# CAPE-OPEN PYTHON UO IMPLEMENTATION: INTRODUCTION

## Key drivers

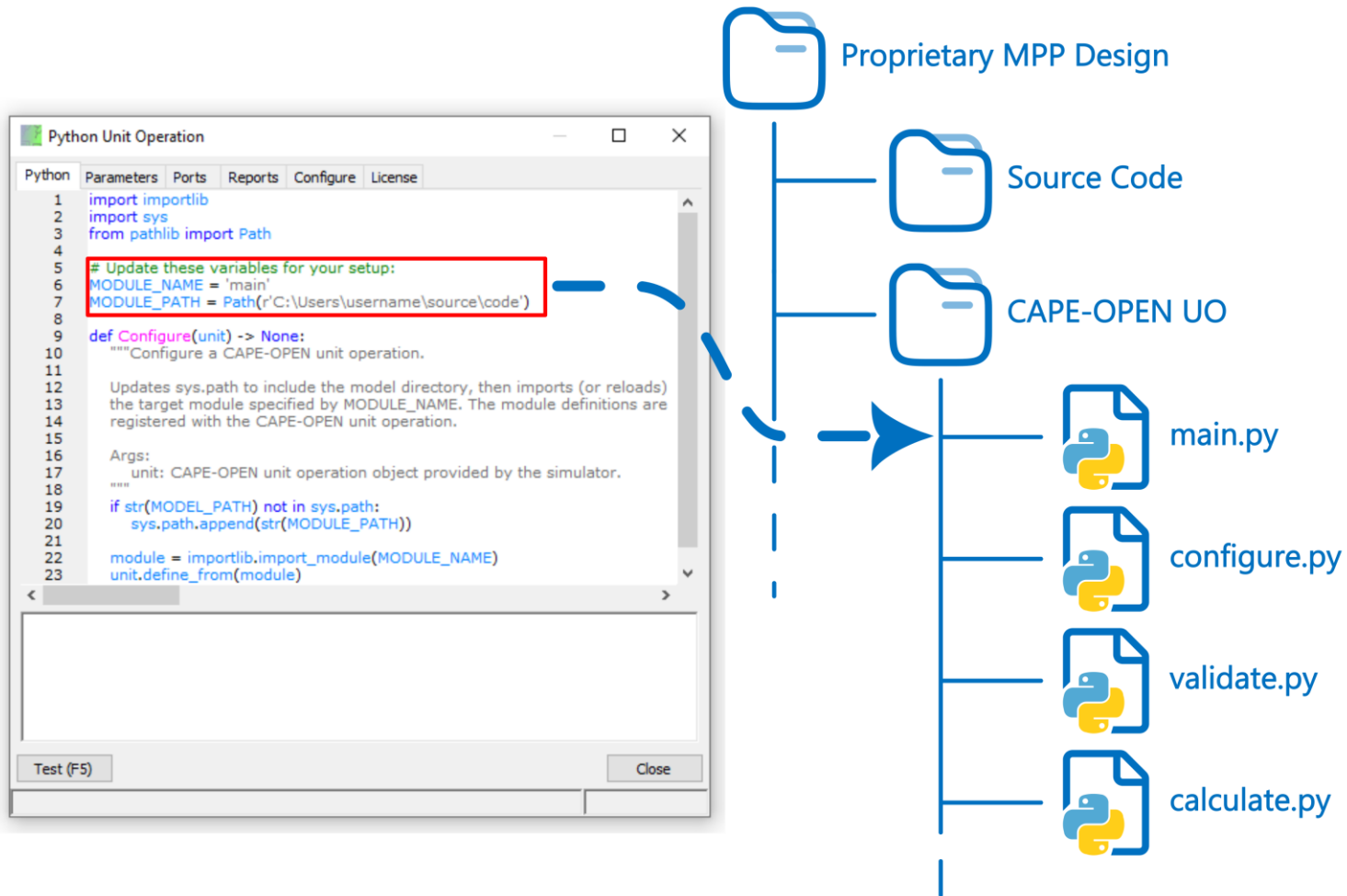
- Ensure thermodynamic model consistency by using the same model as the PME
- Handle complex compositions without further assumptions in the MPP design software
- Execute MPP design software directly through Python to pass the feed object from the PME as the thermodynamic object

## Key constraint

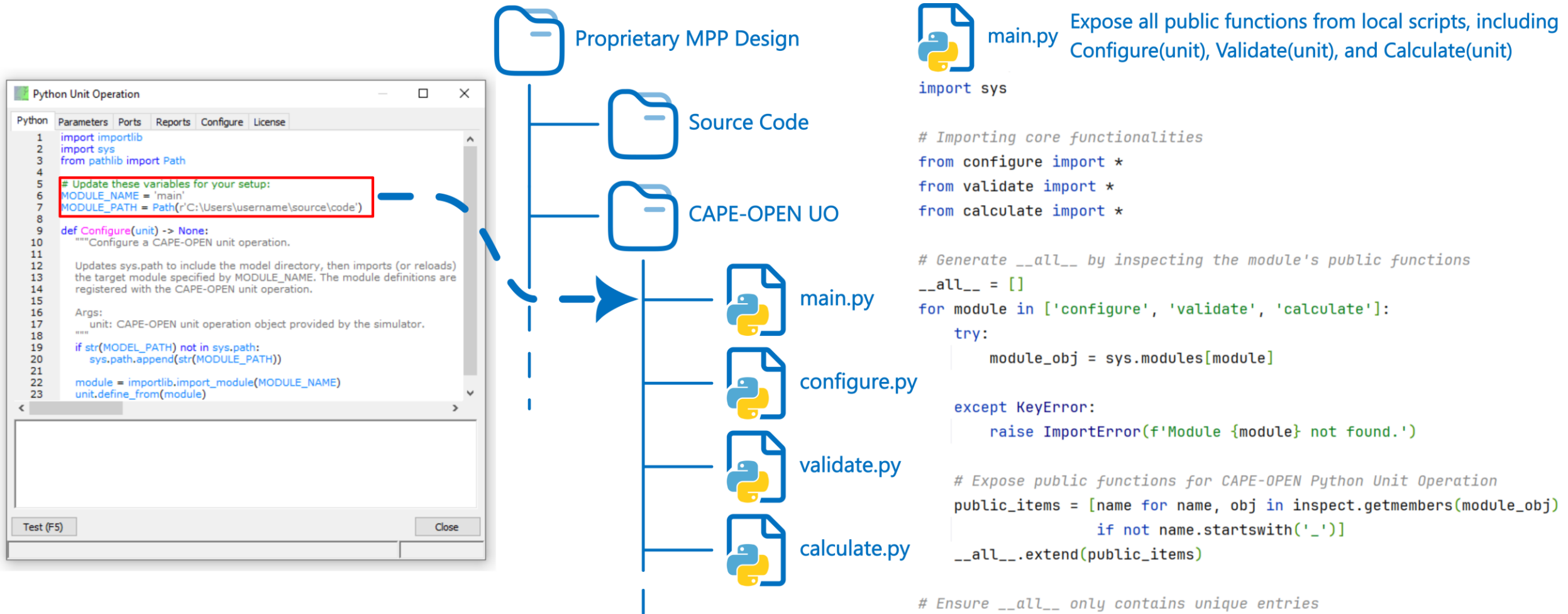
- Address the complexity and multiple dependencies of the MPP design code with a modular implementation
- Deploy the AmsterCHEM CAPE-OPEN Python UO on multiple PMEs: COFE, PRO/II™ & HYSYS®



# CAPE-OPEN PYTHON UO IMPLEMENTATION: INSIGHTS



# CAPE-OPEN PYTHON UO IMPLEMENTATION: INSIGHTS



# CAPE-OPEN PYTHON UO IMPLEMENTATION: FEATURES

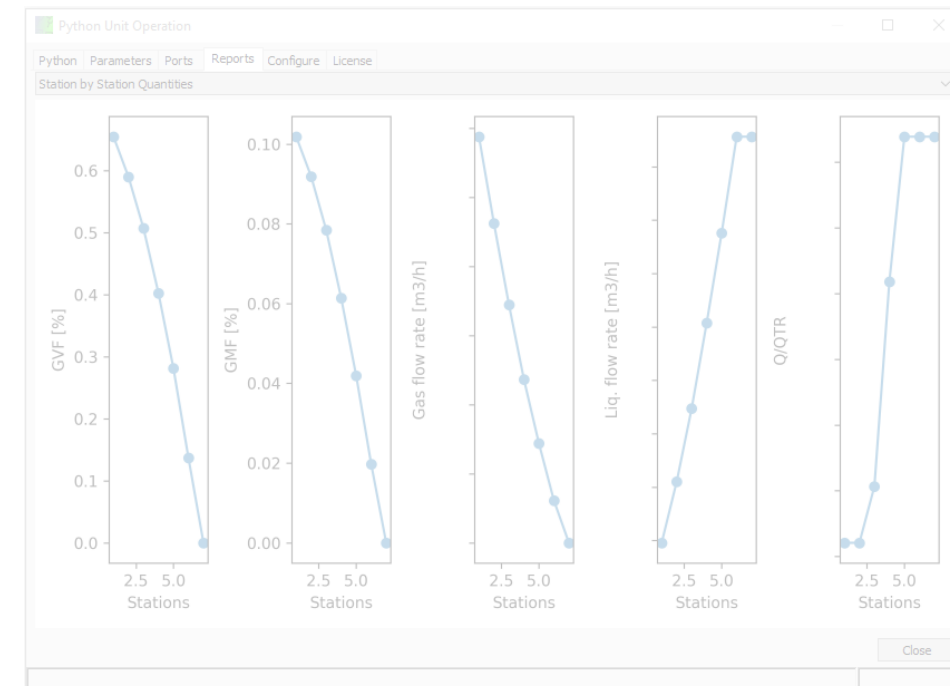
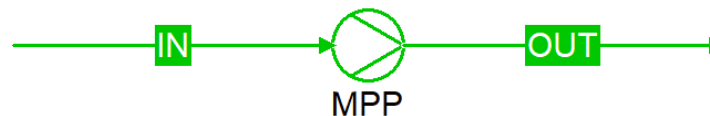
- Calculation applied to CO2 with impurities conditioning with a Multiflash® model
- Facilitates rapid and interactive analyses through the integrated CAPE-OPEN GUI
  - ✓ Fully customizable input settings
  - ✓ Provides direct user access to output visualization through the Reports tab

Unit operation MULTIPHASE PUMP:

| Name                                                  | Status                   | Edit    | Balance | Ports | Streams | Info |
|-------------------------------------------------------|--------------------------|---------|---------|-------|---------|------|
| Parameter                                             | Value                    | Unit    |         |       |         |      |
| Write Results                                         | No                       |         |         |       |         |      |
| Output Path                                           | C:\Users\cariesv\Desktop |         |         |       |         |      |
| Pump Configuration: Configuration Name                | Pump_Design              |         |         |       |         |      |
| Pump Configuration: Rotation Speed                    | 523.598775598            | rad / s |         |       |         |      |
| Flow Type                                             | CO2                      |         |         |       |         |      |
| Pump Design: Type                                     | Stage Optimization       |         |         |       |         |      |
| Pump Design: Exit Condition                           | Full Liquefaction        |         |         |       |         |      |
| Pump Design: Exit Pressure Target                     | 6000000                  | Pa      |         |       |         |      |
| Pump Design: Exit Efficiency Lower Bound              | 0.2                      |         |         |       |         |      |
| Pump Design: Maximum Stage Number                     | 10                       |         |         |       |         |      |
| Stage Optimization: Minimum Flow Multiplier           | 1                        |         |         |       |         |      |
| Stage Optimization: Maximum Flow Multiplier           | 1.15                     |         |         |       |         |      |
| Stage Optimization: Minimum External Diameter         | 0.1                      | m       |         |       |         |      |
| Stage Optimization: Maximum External Diameter         | 0.55                     | m       |         |       |         |      |
| Stage Optimization: Minimum Threshold Constraint o... | 0.95                     |         |         |       |         |      |
| Stage Optimization: Maximum Threshold Constraint o... | 1.2                      |         |         |       |         |      |
| Stage Optimization: Objective Variable                | ETAI                     |         |         |       |         |      |

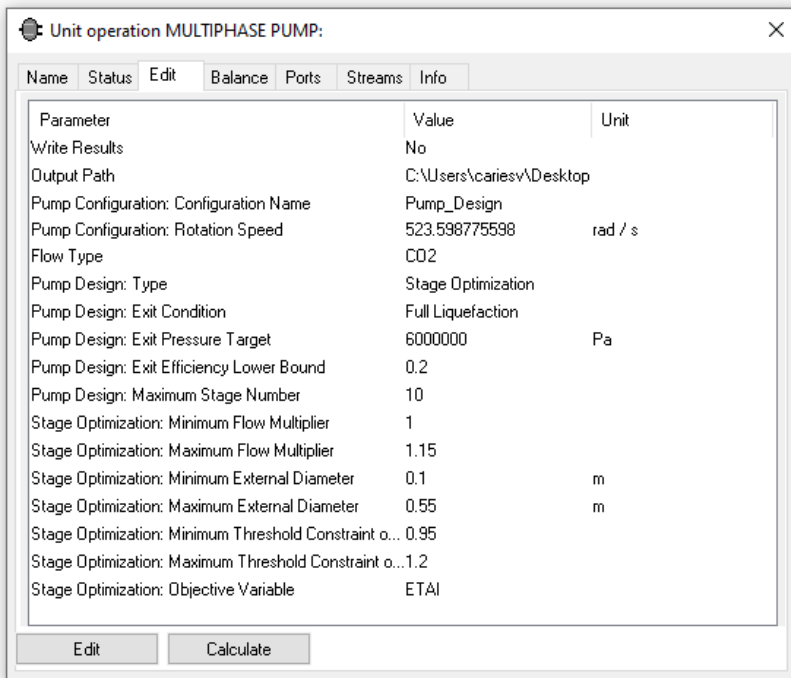
Edit Calculate

| Stream                    | IN     | OUT     | Unit   |
|---------------------------|--------|---------|--------|
| Pressure                  | 25     | 47.75   | bar    |
| Temperature               | -20    | -0.8751 | °C     |
| Flow rate                 | 20     | 20      | kg / s |
| Mole frac CARBON DIOXIDE  | 0.97   | 0.97    |        |
| Mole frac NITROGEN        | 0.015  | 0.015   |        |
| Mole frac ARGON           | 0.01   | 0.01    |        |
| Mole frac OXYGEN          | 0.0025 | 0.0025  |        |
| Mole frac WATER           | 0.0013 | 0.0013  |        |
| Mole frac CARBON MONOXIDE | 0.0012 | 0.0012  |        |
| Vapor phase               |        |         |        |
| phase fraction            | 0.1058 |         |        |
| Liquid phase              |        |         |        |
| phase fraction            | 0.8942 | 1       |        |

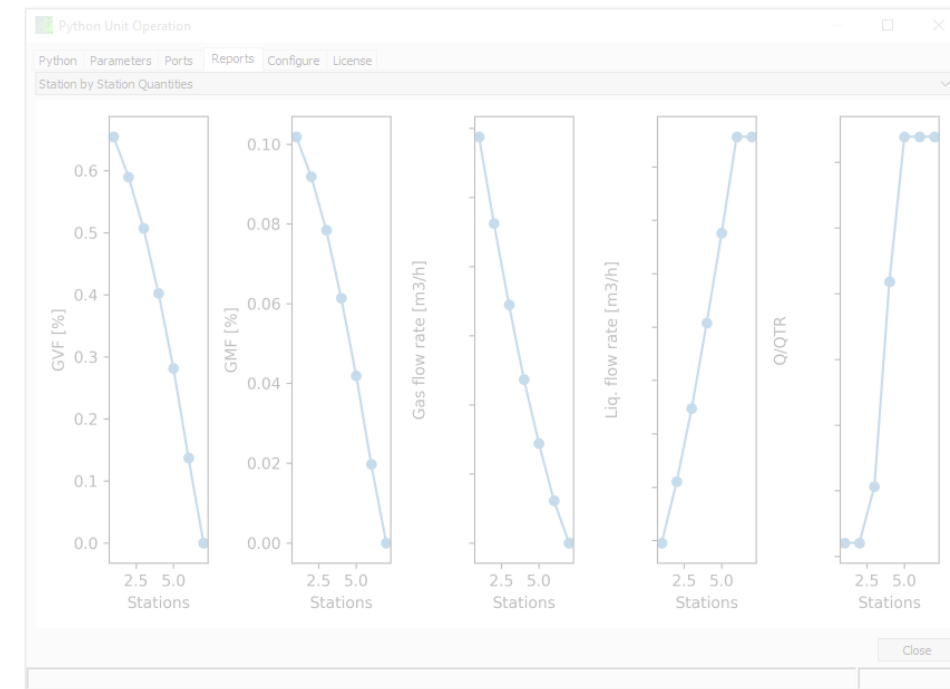
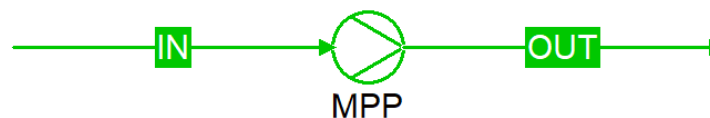


# CAPE-OPEN PYTHON UO IMPLEMENTATION: FEATURES

- Calculation applied to CO2 with impurities conditioning with a Multiflash® model
- Facilitates rapid and interactive analyses through the integrated CAPE-OPEN GUI
  - ✓ Fully customizable input settings
  - ✓ Provides direct user access to output visualization through the Reports tab

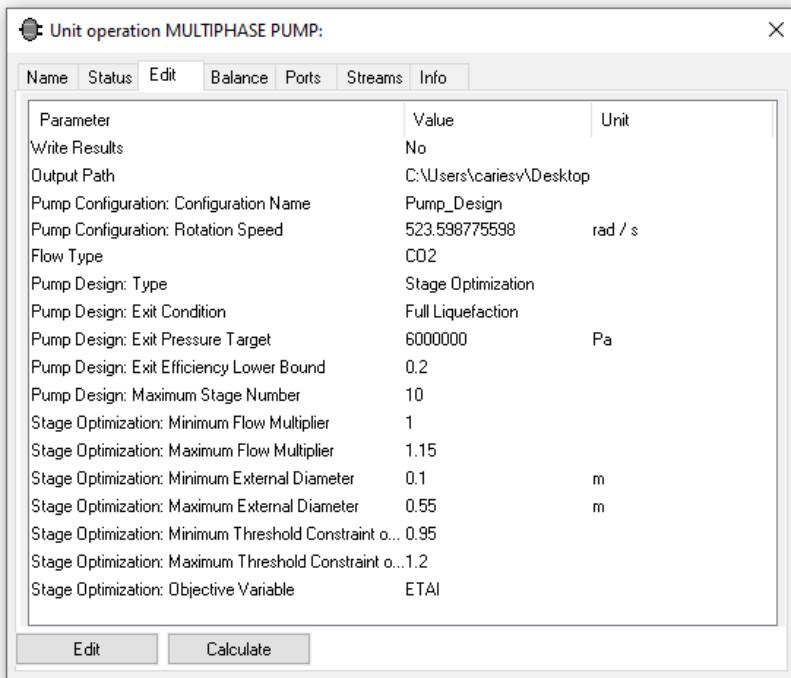


| Stream                    | IN     | OUT     | Unit   |
|---------------------------|--------|---------|--------|
| Pressure                  | 25     | 47.75   | bar    |
| Temperature               | -20    | -0.8751 | °C     |
| Flow rate                 | 20     | 20      | kg / s |
| Mole frac CARBON DIOXIDE  | 0.97   | 0.97    |        |
| Mole frac NITROGEN        | 0.015  | 0.015   |        |
| Mole frac ARGON           | 0.01   | 0.01    |        |
| Mole frac OXYGEN          | 0.0025 | 0.0025  |        |
| Mole frac WATER           | 0.0013 | 0.0013  |        |
| Mole frac CARBON MONOXIDE | 0.0012 | 0.0012  |        |
| Vapor phase               |        |         |        |
| phase fraction            | 0.1058 |         |        |
| Liquid phase              |        |         |        |
| phase fraction            | 0.8942 | 1       |        |

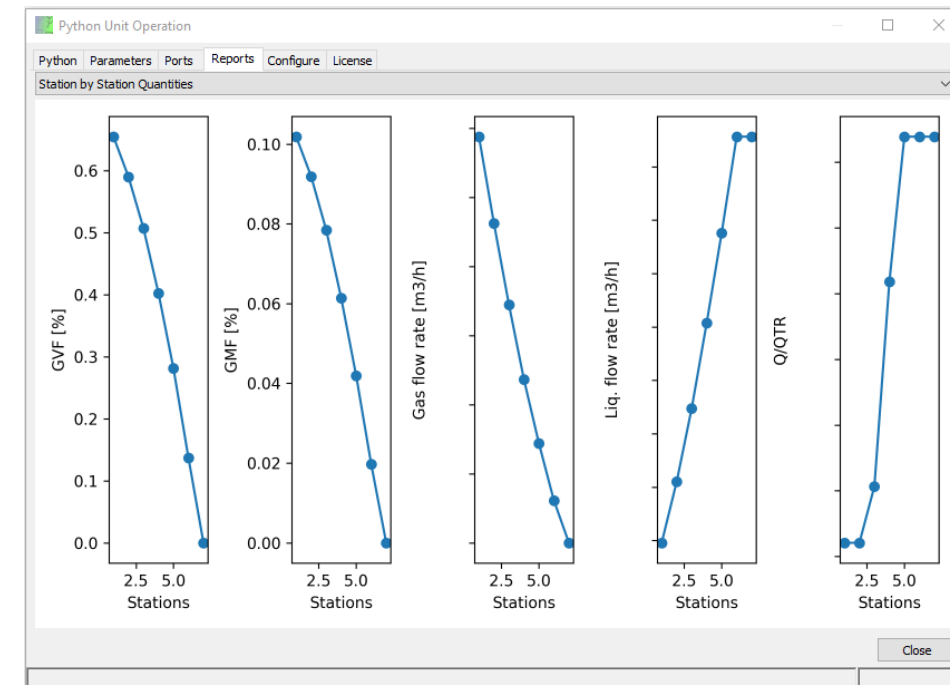
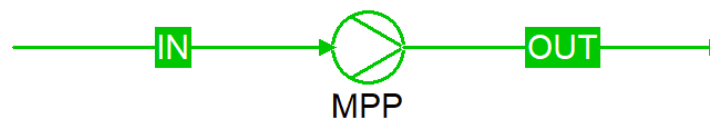


# CAPE-OPEN PYTHON UO IMPLEMENTATION: FEATURES

- Calculation applied to CO2 with impurities conditioning with a Multiflash® model
- Facilitates rapid and interactive analyses through the integrated CAPE-OPEN GUI
  - ✓ Fully customizable input settings
  - ✓ Provides direct user access to output visualization through the Reports tab



| Stream                    | IN     | OUT     | Unit   |
|---------------------------|--------|---------|--------|
| Pressure                  | 25     | 47.75   | bar    |
| Temperature               | -20    | -0.8751 | °C     |
| Flow rate                 | 20     | 20      | kg / s |
| Mole frac CARBON DIOXIDE  | 0.97   | 0.97    |        |
| Mole frac NITROGEN        | 0.015  | 0.015   |        |
| Mole frac ARGON           | 0.01   | 0.01    |        |
| Mole frac OXYGEN          | 0.0025 | 0.0025  |        |
| Mole frac WATER           | 0.0013 | 0.0013  |        |
| Mole frac CARBON MONOXIDE | 0.0012 | 0.0012  |        |
| Vapor phase               |        |         |        |
| phase fraction            | 0.1058 |         |        |
| Liquid phase              |        |         |        |
| phase fraction            | 0.8942 | 1       |        |



# CAPE-OPEN PYTHON UO IMPLEMENTATION: AVAILABLE ON PMEs



COFE



AVEVA™ PRO/II™

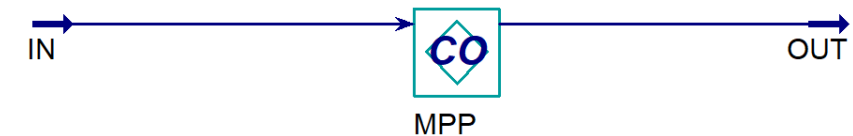
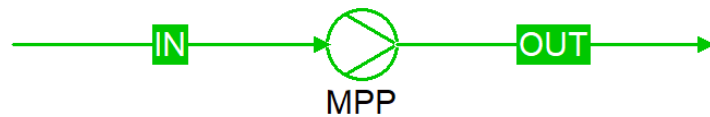


Aspen HYSYS®

| Stream                    | IN     | OUT     | Unit   |
|---------------------------|--------|---------|--------|
| Pressure                  | 25     | 47.75   | bar    |
| Temperature               | -20    | -0.8751 | °C     |
| Flow rate                 | 20     | 20      | kg / s |
| Mole frac CARBON DIOXIDE  | 0.97   | 0.97    |        |
| Mole frac NITROGEN        | 0.015  | 0.015   |        |
| Mole frac ARGON           | 0.01   | 0.01    |        |
| Mole frac OXYGEN          | 0.0025 | 0.0025  |        |
| Mole frac WATER           | 0.0013 | 0.0013  |        |
| Mole frac CARBON MONOXIDE | 0.0012 | 0.0012  |        |
| Vapor phase               |        |         |        |
| phase fraction            | 0.1058 |         |        |
| Liquid phase              |        |         |        |
| phase fraction            | 0.8942 | 1       |        |

| Stream Name          |           | IN        | OUT       |
|----------------------|-----------|-----------|-----------|
| Stream Description   |           | Mixed     | Liquid    |
| Phase                |           |           |           |
| Temperature          | C         | -20,0000  | -0,8750   |
| Pressure             | BAR       | 25,0000   | 47,7469   |
| Enthalpy             | M*KJ/HR   | -22,9721  | -21,3251  |
| Molecular Weight     |           | 43,6462   | 43,6462   |
| Mole Fraction Vapor  |           | 0,1058    | 0,0000    |
| Mole Fraction Liquid |           | 0,8942    | 1,0000    |
| Rate                 | KG-MOL/HR | 1649,627  | 1649,627  |
| Fluid Rates          | KG-MOL/HR |           |           |
| CO2                  |           | 16,4963   | 16,4963   |
| CO2                  |           | 1600,1387 | 1600,1387 |
| N2                   |           | 24,7444   | 24,7444   |
| O2                   |           | 4,1241    | 4,1241    |
| H2O                  |           | 2,1445    | 2,1445    |
| CO                   |           | 1,9796    | 1,9796    |

| Material Streams   |          |             |             |
|--------------------|----------|-------------|-------------|
|                    |          | IN          | OUT         |
| Vapour Fraction    |          | 0,1058      | 0,0000      |
| Temperature        | C        | -20,00      | -0,8749     |
| Pressure           | kPa      | 2500        | 4775        |
| Molar Flow         | kgmole/h | 1650        | 1650        |
| Mass Flow          | kg/h     | 7,200e+004  | 7,200e+004  |
| Liquid Volume Flow | m3/h     | 86,89       | 86,89       |
| Heat Flow          | kJ/h     | -6,534e+008 | -6,517e+008 |



# CAPE-OPEN PYTHON UO IMPLEMENTATION: AVAILABLE ON PMEs



COFE



AVEVA™ PRO/II™

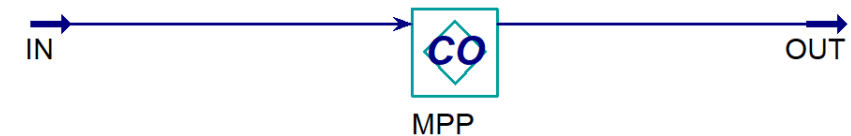
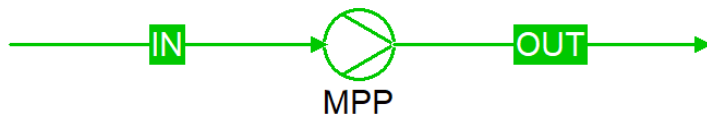


Aspen HYSYS®

| Stream                    | IN     | OUT     | Unit   |
|---------------------------|--------|---------|--------|
| Pressure                  | 25     | 47.75   | bar    |
| Temperature               | -20    | -0.8751 | °C     |
| Flow rate                 | 20     | 20      | kg / s |
| Mole frac CARBON DIOXIDE  | 0.97   | 0.97    |        |
| Mole frac NITROGEN        | 0.015  | 0.015   |        |
| Mole frac ARGON           | 0.01   | 0.01    |        |
| Mole frac OXYGEN          | 0.0025 | 0.0025  |        |
| Mole frac WATER           | 0.0013 | 0.0013  |        |
| Mole frac CARBON MONOXIDE | 0.0012 | 0.0012  |        |
| Vapor phase               |        |         |        |
| phase fraction            | 0.1058 |         |        |
| Liquid phase              |        |         |        |
| phase fraction            | 0.8942 | 1       |        |

| Stream Name          |           | IN        | OUT       |
|----------------------|-----------|-----------|-----------|
| Stream Description   |           | Mixed     | Liquid    |
| Phase                |           |           |           |
| Temperature          | C         | -20,0000  | -0,8750   |
| Pressure             | BAR       | 25,0000   | 47,7469   |
| Enthalpy             | M*KJ/HR   | -22,9721  | -21,3251  |
| Molecular Weight     |           | 43,6462   | 43,6462   |
| Mole Fraction Vapor  |           | 0,1058    | 0,0000    |
| Mole Fraction Liquid |           | 0,8942    | 1,0000    |
| Rate                 | KG-MOL/HR | 1649,627  | 1649,627  |
| Fluid Rates          |           |           |           |
| CO2                  | KG-MOL/HR | 16,4963   | 16,4963   |
| CO2                  |           | 1600,1387 | 1600,1387 |
| N2                   |           | 24,7444   | 24,7444   |
| O2                   |           | 4,1241    | 4,1241    |
| H2O                  |           | 2,1445    | 2,1445    |
| CO                   |           | 1,9796    | 1,9796    |

| Material Streams   |          |             |             |
|--------------------|----------|-------------|-------------|
|                    |          | IN          | OUT         |
| Vapour Fraction    |          | 0,1058      | 0,0000      |
| Temperature        | C        | -20,00      | -0,8749     |
| Pressure           | kPa      | 2500        | 4775        |
| Molar Flow         | kgmole/h | 1650        | 1650        |
| Mass Flow          | kg/h     | 7,200e+004  | 7,200e+004  |
| Liquid Volume Flow | m3/h     | 86,89       | 86,89       |
| Heat Flow          | kJ/h     | -6,534e+008 | -6,517e+008 |



✓ Proprietary MPP design code successfully integrated in COFE, PRO/II™ & HYSYS® using AmsterCHEM CAPE-OPEN Python UO



# CAPE-OPEN PYTHON UO IMPLEMENTATION: USER FEEDBACK

## Strengths

- User-friendly CAPE-OPEN formalism with easy implementation via clear documentation
- COFE: ideal for prototyping and testing new features

## Challenges

- Adding Python virtual environment support would make it easier to address package compatibility challenges in large Python projects
- PRO/II™: missing phase related feed stream properties that should be available
- HYSYS®: requires changing the unit CapeVersion in the registry to 1.1 (misunderstanding of the standard) and lacks essential feed stream properties

**Acknowledgments:** a big thanks to J. Van Baten for the CAPE-OPEN Python UO 1.0.26.0 release addressing the missing properties issue in PRO/II™ & HYSYS®



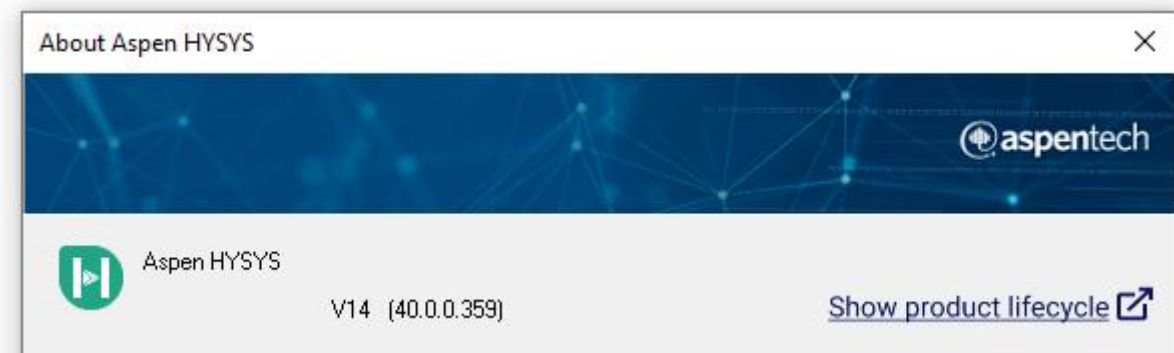
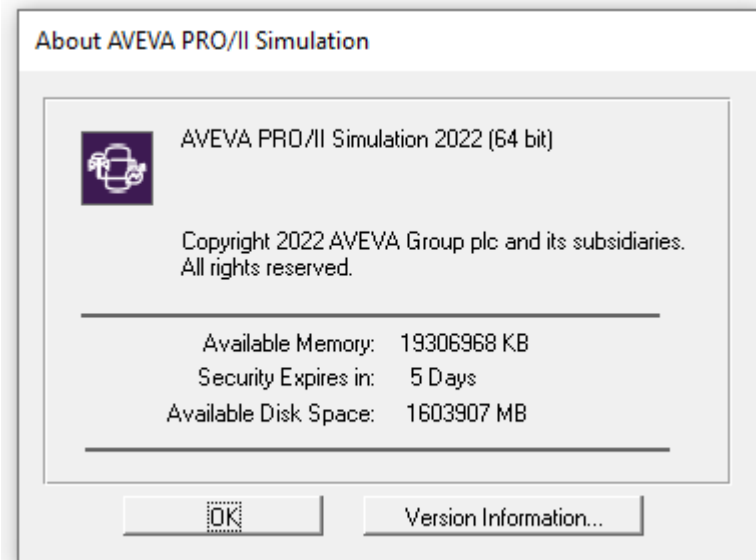
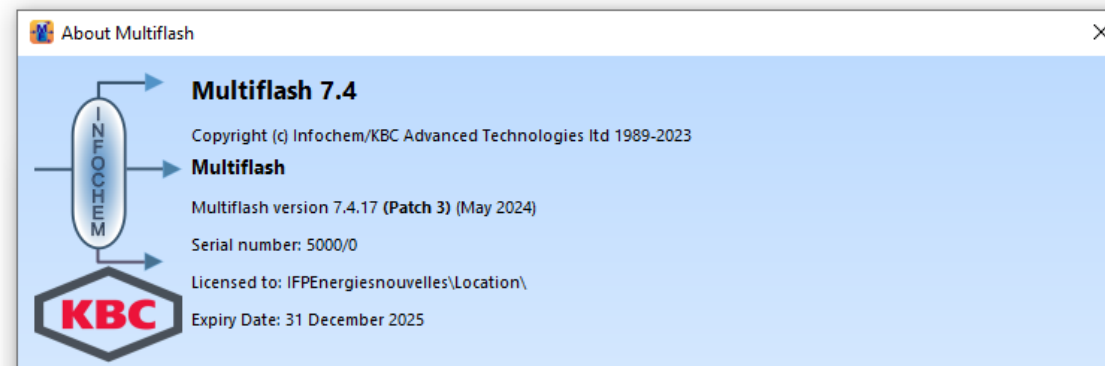
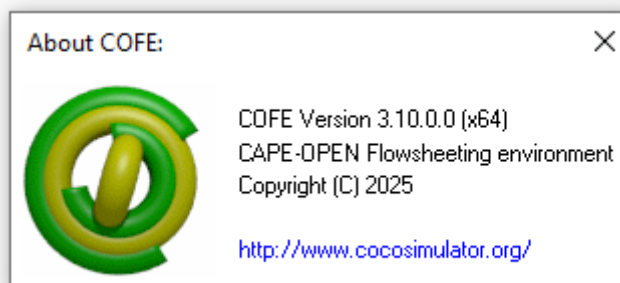
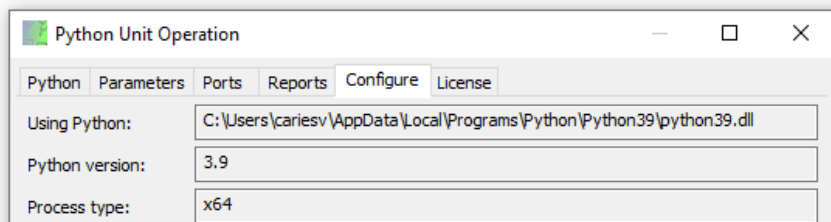
# CONCLUSIONS & PERSPECTIVES

## CONCLUSIONS & PERSPECTIVES

- ✓ **Proprietary MPP design software successfully integrated in COFE, PRO/II™ & HYSYS® using the AmsterCHEM CAPE-OPEN Python UO**
- ✓ **Thermodynamic model consistency:** ensured by being able to use the same model as the PME
- ✓ **Integration into complex process flowsheets:** enabled by treating the MPP as a standard pump component
- ✓ **Easier collaboration** during new process design and exploration phases
- **Enhancing the robustness of the MPP design software** to effectively handle unexplored configurations
- **Improving error handling** between the MPP design software and the CAPE-OPEN standard for smoother operation

# REFERENCES

Python Unit Operation license  
Version 1.0.26.0  
Copyright (C) AmsterCHEM 2025





*Innovating for a low-carbon  
and sustainable world*

[www.ifpenergiesnouvelles.com](http://www.ifpenergiesnouvelles.com)

### **IFP Energies nouvelles**

1 - 4 avenue de Bois-Préau  
92852 Rueil-Malmaison Cedex - France

Tel.: +33 1 47 52 60 00

### **IFP Energies nouvelles**

Rond-point de l'échangeur de Solaize  
BP 3 – 69360 Solaize - France

Tel.: +33 4 37 70 20 00