

Process synthesis of advanced NH₃ and MeOH plants with gas switching reforming (GSR)

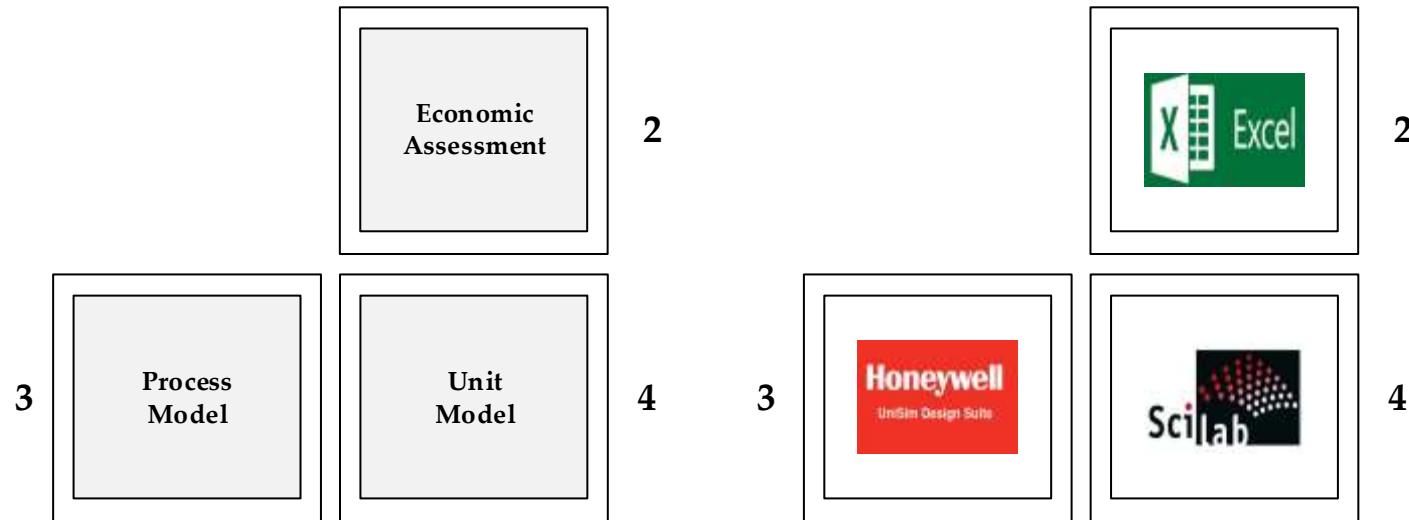
Carlos Arnaiz del Pozo

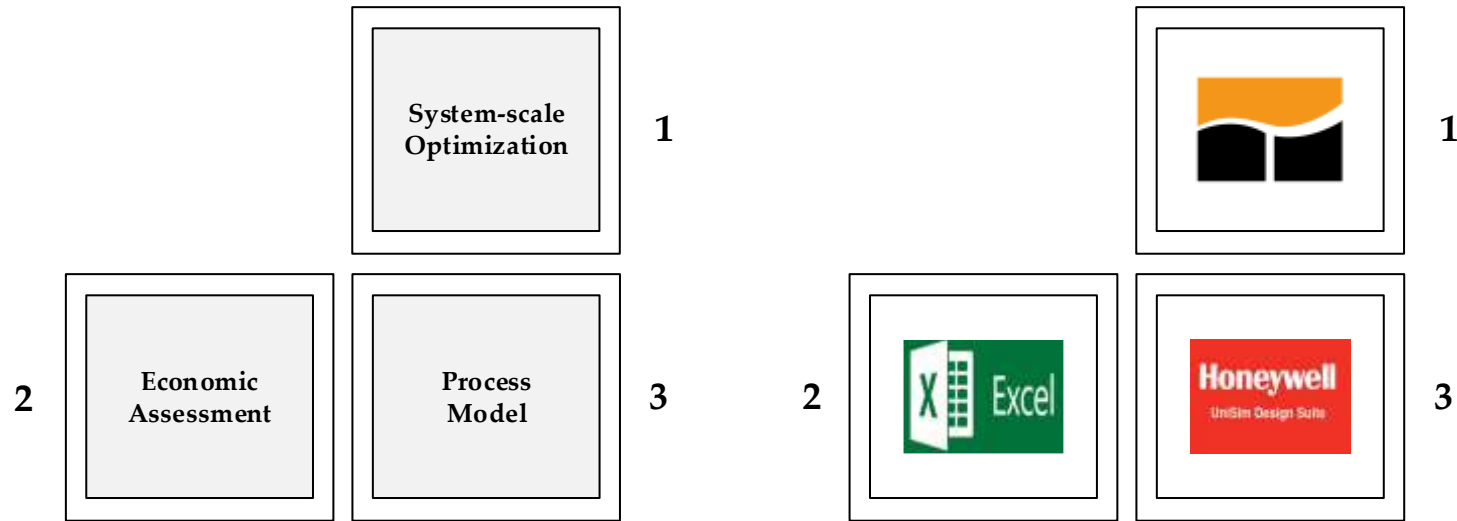
Schalk Cloete

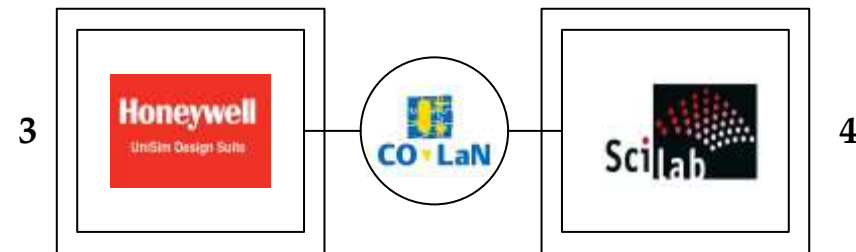
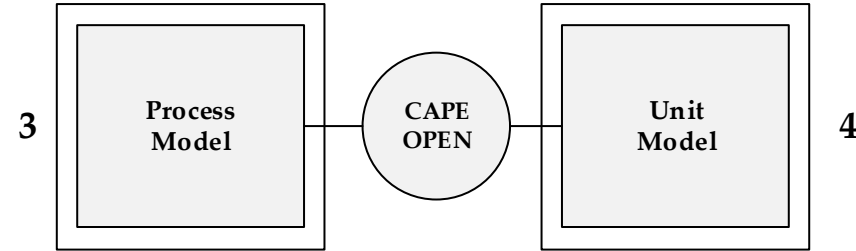
Ángel Jiménez Álvaro



Margarita Salas grant, NextGeneration EU, Ministerio de Universidades ref. RD 289/2021

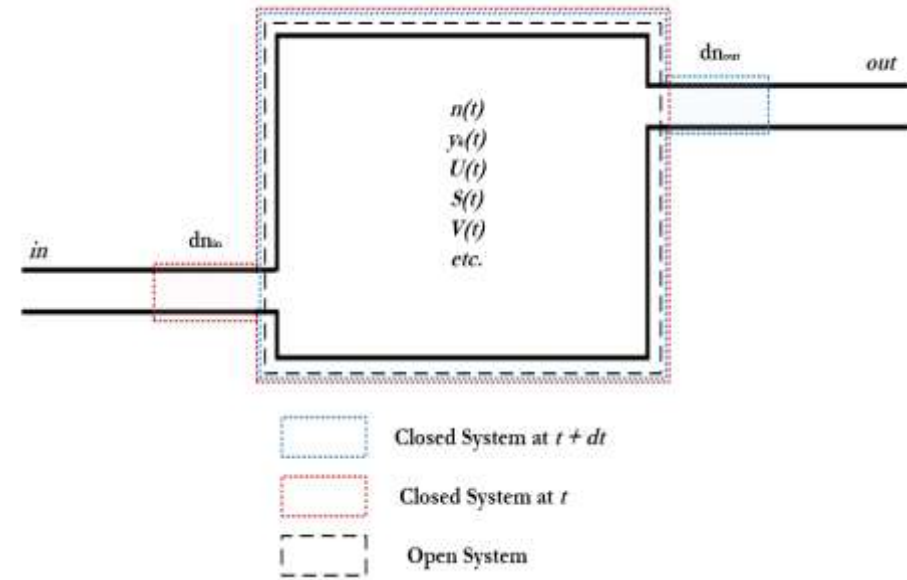


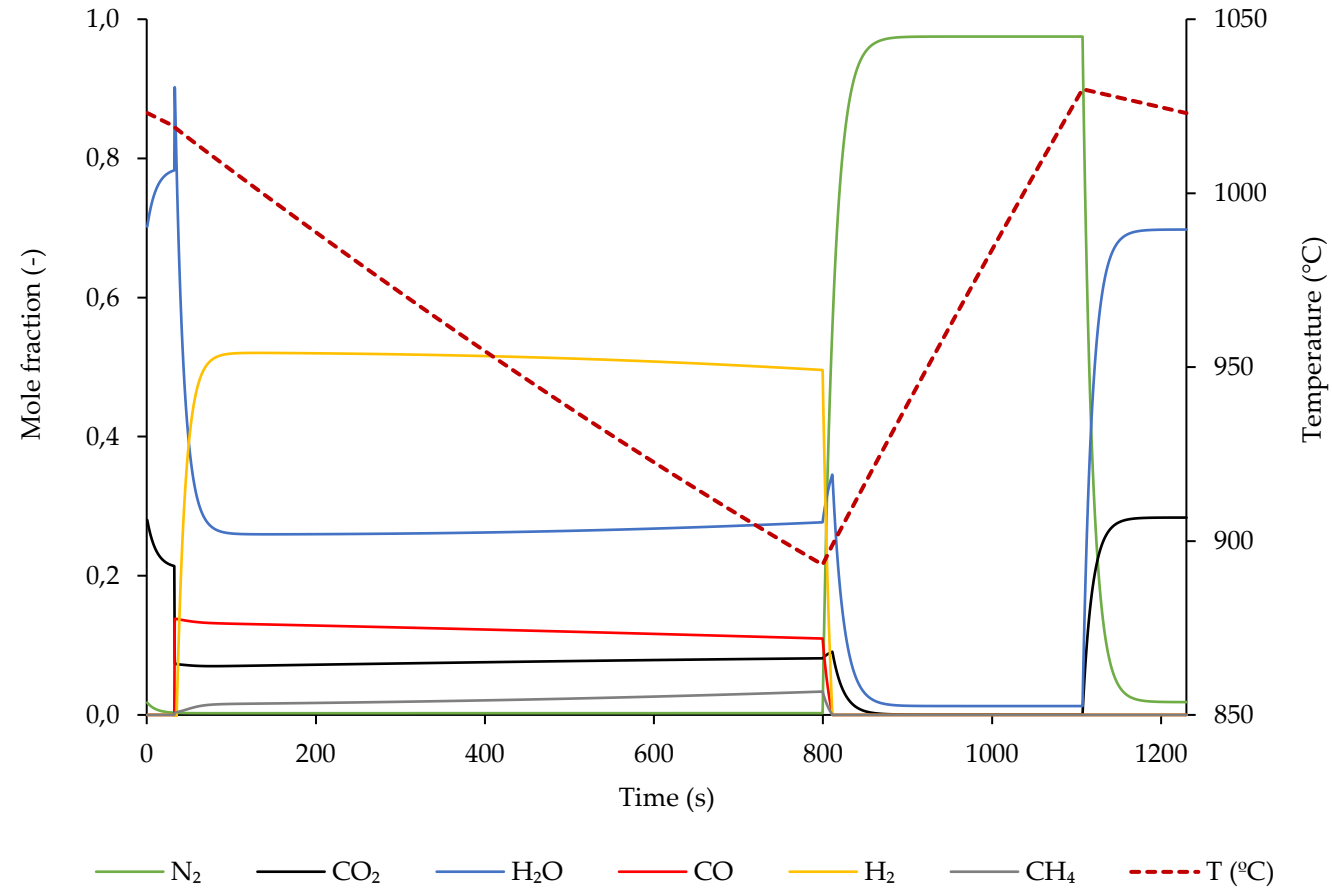




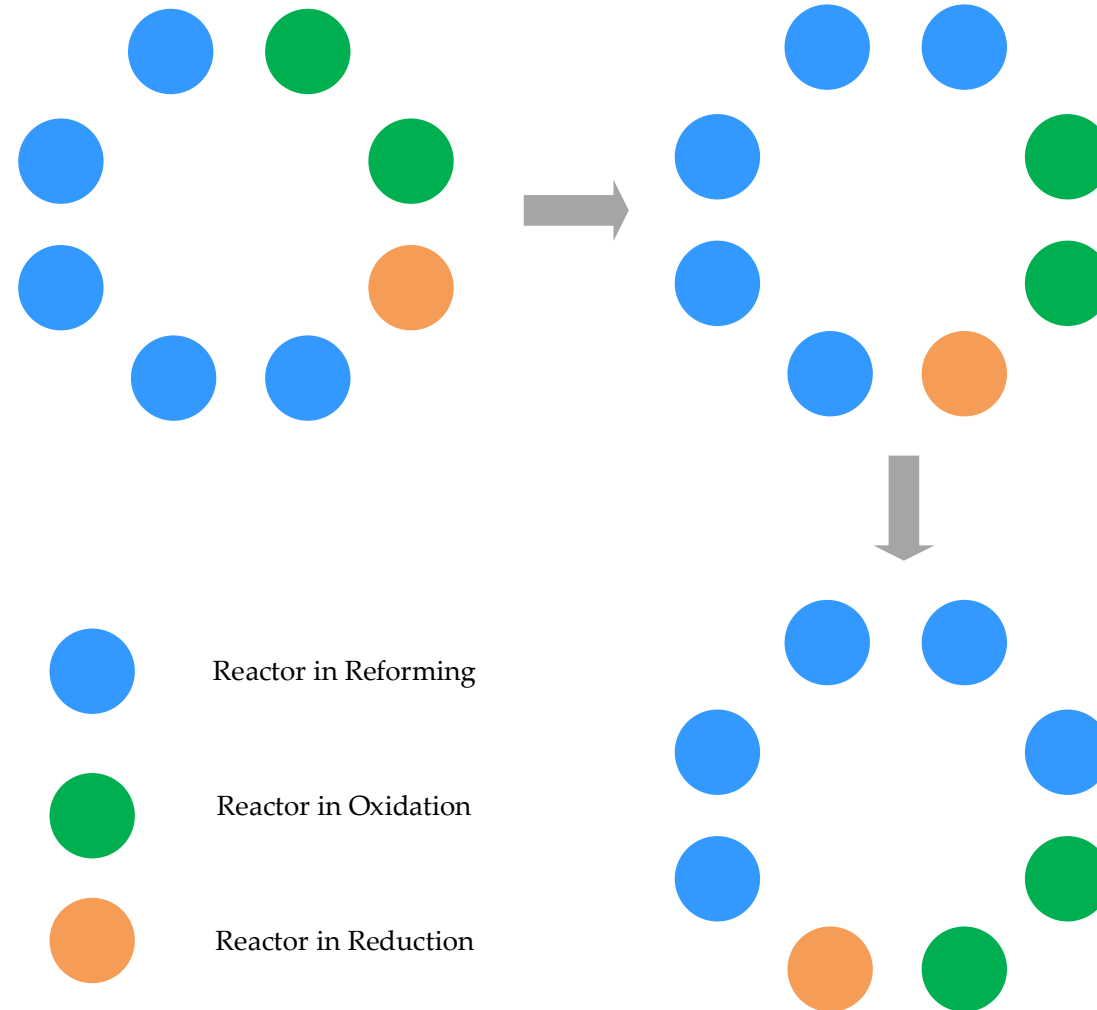
GSR reactor

Mass Balance	$\frac{dn_k}{dt} = F_{in}y_{in,k} + F_{out}y_{out,k} + \sum_{r=1}^R \nu_{r,k}\xi_r$
Energy Balance	$\frac{dT}{dt} = \frac{-F_{in} \sum_k y_{in,k} \int_{T_{in}}^T c_{p,k} dT + \sum_{r=1}^R \xi_r (-\Delta H_{r,T})}{\sum_k n_k c_{p,k}}$
Outlet flow	$F_{out} = F_{in} + \sum_{k \in gases} \nu_{k,r} \xi_r + \frac{PV_{gas}}{RT^2} \dot{T}$

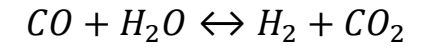
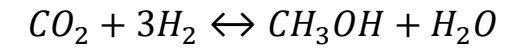
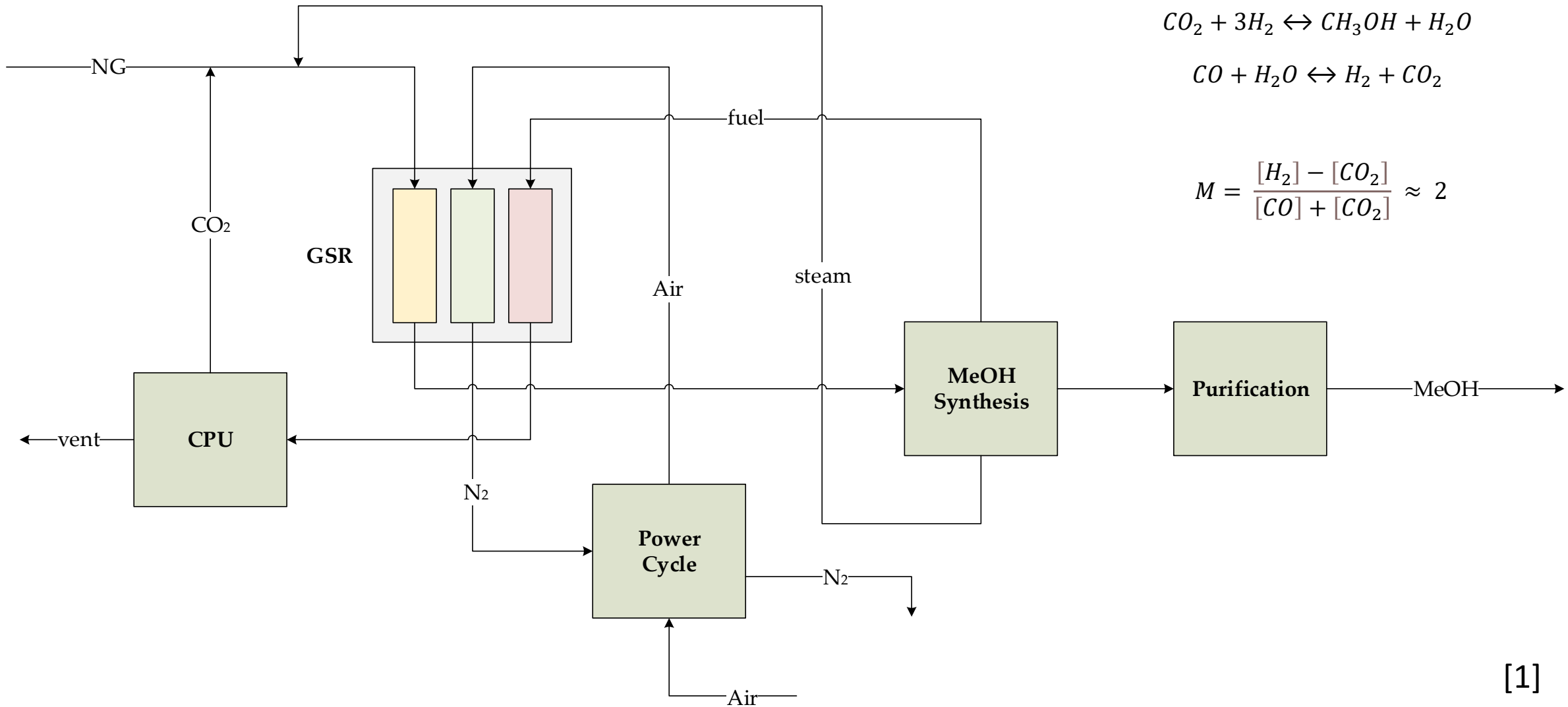




GSR cluster

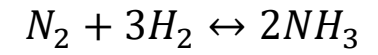


GSR-MeOH

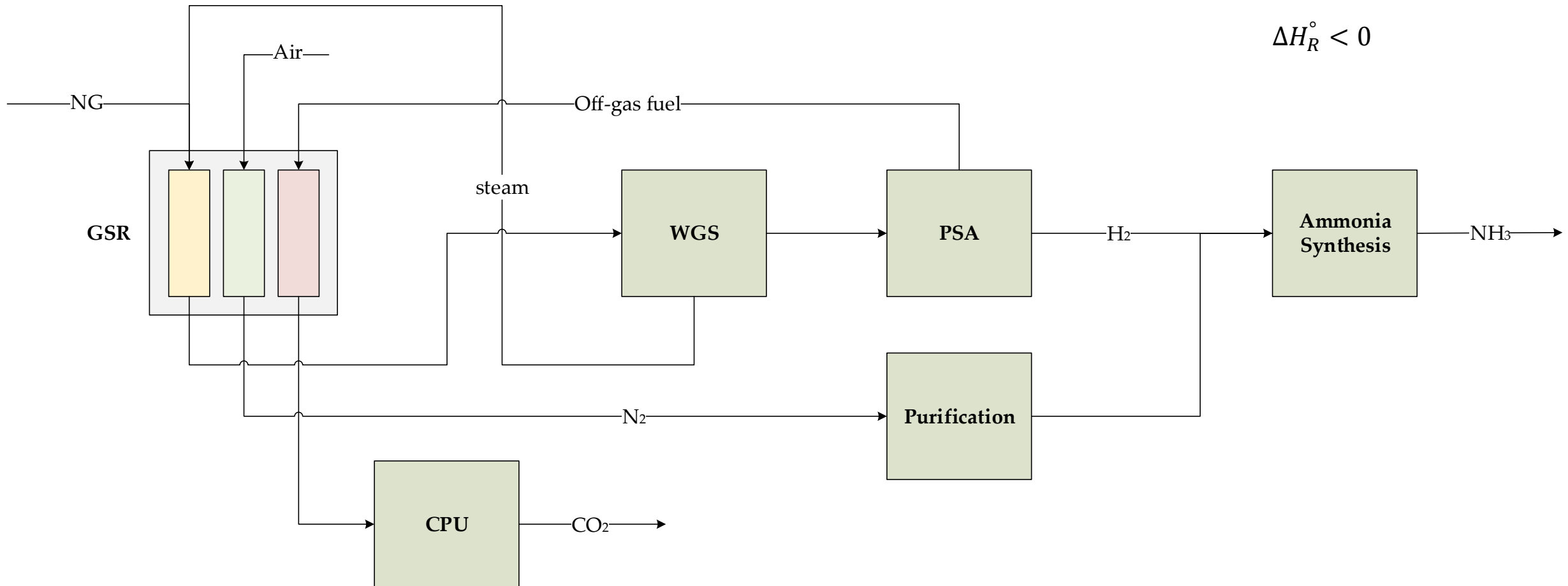


$$M = \frac{[H_2] - [CO_2]}{[CO] + [CO_2]} \approx 2$$

GSR-NH₃



$$\Delta H_R^\circ < 0$$

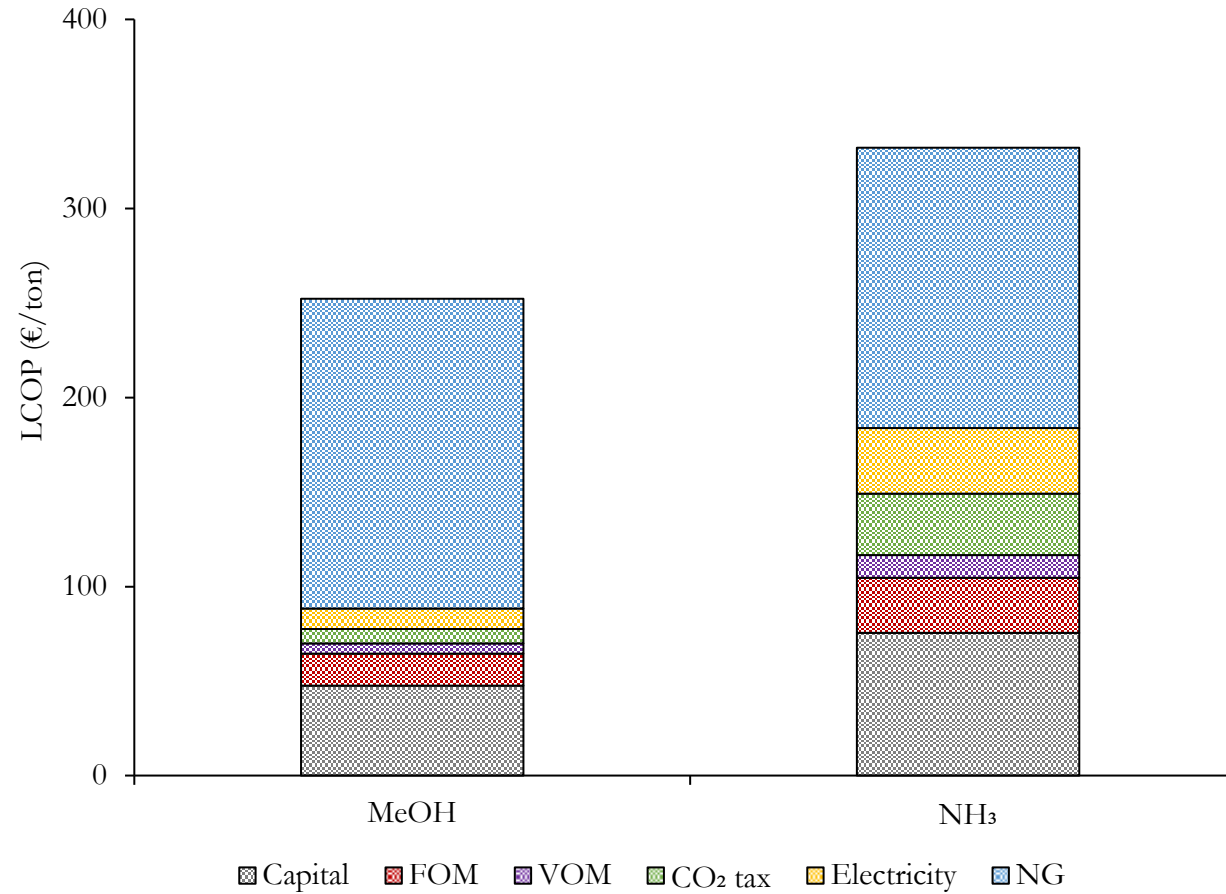


CAPE-OPEN unit

1. getFeedProp
2. getParameter
3. setProduct

Input	Output
Air	N ₂
Fuel	Reduction gases
Natural gas	Syngas
n° of reactors	fl. velocities

Results



Conclusions

- CAPE-OPEN Unisim Design – Scilab unit operation
- Transient gas switching reforming (GSR) model connected to stationary plant
- GSR model can be specified in process flowsheet
- Research output: 7 (9)

References

- [1] C. Arnaiz del Pozo, S. Cloete and Á Jiménez Álvaro, "Techno-economic assessment of long-term methanol production from natural gas and renewables" *Energy Conversion and Management*. 2022, vol. 266, pp. 115785.
- [2] C. Arnaiz del Pozo and S. Cloete, "Techno-economic assessment of blue and green ammonia as energy carriers in a low-carbon future" *Energy Conversion and Management*. 2022, vol. 255, pp. 115312.
- [3] Carlos Arnaiz del Pozo, Schalk Cloete, and Ángel Jiménez Álvaro. Standard Economic Assessment (SEA) Tool. Available from: <https://bit.ly/3hyF1TT>.