



Beyond Compliance

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Assuring CAPE-OPEN Adoption

- A set of standardized interfaces are in place and have been implemented by multiple vendors
- Widespread adoption/use of these interfaces will depend upon more than technical feasibility and availability





Adoption Issues

- Quality of implementation in Process Modeling Environment (PME)
- PME interface capabilities
- Interface experience

Ideally user should not even notice that CAPE-OPEN interfaces are being used.





Implementation Quality

- Implementation should be as seamless as possible
 - Maximize existing knowledge of PME
- Exploit capabilities of PME





Implementation Quality (HTRI)

- Implemented Unit Operation interface for three most used Xchanger Suite modules
 - Xist (Shell and Tube)
 - Xace (Air-coolers/Economizers)
 - Xphe (Plate and frame)
- Implemented Thermodynamic interface within Xchanger Suite
- Tested against multiple process simulators and property packages





Implementation Quality (HTRI)

- Xchanger Suite calculation modules evolved as stand alone engines
 - Optimized for rigor instead of calculation speed
 - Fluid property handling modified
 - Known versus unknown duty
 - Significant input/runtime problems result in diagnostic messages and end of calculations
 - Process condition handling not consistent with most process simulators
 - HTRI based on property grid
 - Simulators provide temperature and vapor fraction which may be inconsistent with interpolated conditions



Property Options

Floperty deneration		
Generate new properties during run		
Number of pressure sets Default	Temperature increment method	Equal Fraction 🔻
Number of temperature points Default	Flash type	Integral
Adjust calculated points	Supercritical Conditions	
✓ Insert bubble point if in temperature range	Critical pressure	psia
 ✓ Insert dew point if in temperature range ✓ Generate component fractions 	Supercritical phase	Liquid 🔻
Starting Temperature	Starting Pressure	
C Use inlet temperature	C Use inlet pressure	
© Use temperature F	 Use pressure 	psia
Ending Temperature	Ending Pressure	
 Use opposite stream inlet temperature 	 Use calculated pressu 	ure
C Use calculated outlet temperature	Pres. drop estimate	psi
Temperature estimate F	C Use pressure	psia
C Use temperature F	C Use pressure drop	psi



PME Capabilities



- Reporting
- Unit operation interface







17 18	PARAMETERS								
19 20		Exchanger Design (End Point)							
21	Tube Side DeltaP:	0.6895 kPa *	895 kPa * Shell Side DeltaP: 68.95 kPa * Passes:			Passes:			
22	UA:	845.7 kJ/C-h							
23		Гube Side Data					Shell Side Data		
24	Heat Transfer Coefficient				Heat Transfer Coefficient				
25	Tube Pressure Drop			0.69 kPa *	Shell Pressure Drop			68.95 kPa *	
26	Fouling		0.0	0000 C-h-m2/kJ *	Fouling			0.00000 C-h-m2/kJ *	
27	Tube Length			1.00 m *	Shell Passes			1	
28	Tube O.D.			20.00 mm *	Shell Series			1 *	
29	Tube Thickness		2.0000 mm		Shell Parallel			1 *	
30				50.0000 mm *	Baffle Type			Single	
31	Orientation		Horizontal		Baffle Cut(%Area)			20.00 *	
32	Passes Per Shell		1 *		Baffle Orientation			Horizontal	
33			80 *		Spacing			800.0000 mm *	
34			Triangular (30 degrees)		Diameter			530.0259 mm *	
35	ТЕМА Туре		AEL		Area			5.03 m2	
36 37	SPECS								
38		Specified Value	e	Current	: Value	F	Relative Error	Active	Estimate
39	Heat Balance	0.0	0000 kJ/h		1.279e-010 kJ/h		-3.553e-014	On	On
40	UA				845.7 kJ/C-h			On	On
41	'	B (11 1 1 B 1 1 C 1 C 1 C 1 C 1 C 1 C 1 C							
42	Detailed Specifications								
43									
44	Type: Duty		Pass: Er				Spec Value: 0.0000 kJ/h		
45	n.								
46	Type: UA		Pass: Overall Spec Value:						







偃 CO-100			×				
			•				
General properties							
Unit Type	HtriC0100.Xist						
Unit Name	CO-100						
Unit description	CAPE-OPEN (1-0-0) for HTRI's Xist s	shell and tube heat exchanger program	<u>^</u>				
Report result from LAS	Report to be integrated in the HYSYS Report Output Summary Report result from LAST unit execution						
Performance							
Overdesign, % Overall U, W/m2-K Required U, W/m2-K Duty, MegaWatts Shellside h, W/m2-K Tubeside h, W/m2-K Shellside delta P, kP	5.4213 611.46 231.44		*				
<			<u> </u>				
Material Connections	Unit Variables	General	Thermo				
	Solved		Show Unit GUI				



Reporting



Honeywell	■■ HONEYWELL	Case Name:	E:\Cape-Open\Samples\Sample Xist CO Case.hsc			
	Calgary, Alberta	Unit Set:	SI			
	CANADA	Date/Time:	Sunday Feb 12 2006, 10:16:07			
E-OPEN Unit 1.0 Operations: CO-100						
9	(No Datasheets exist for this unit operation)					
10						
11						
12						
13						
15						
16						
12 13 14 15 16 17						
18						

Can CAPE-OPEN access the native reporting mechanisms?



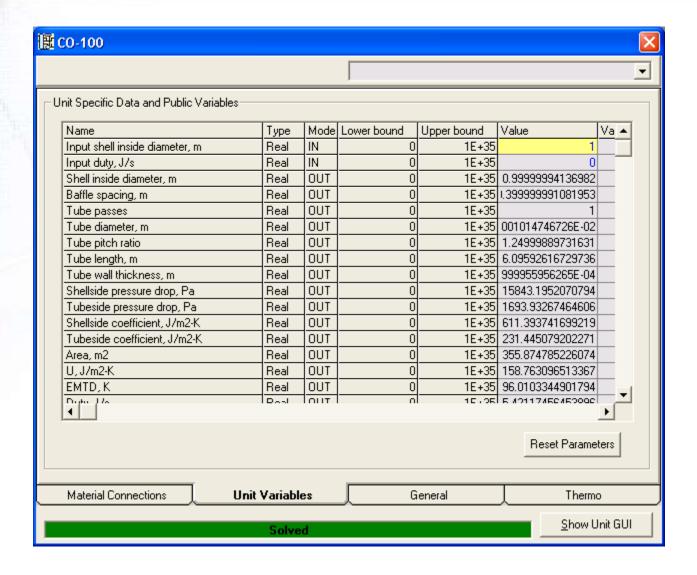


Unit Operation Interface

- Access allowed to native unit operation interface
 - Required for complete control of unit operation
- Allows population of parameters in PME
 - Necessary for PME access to unit operation parameters

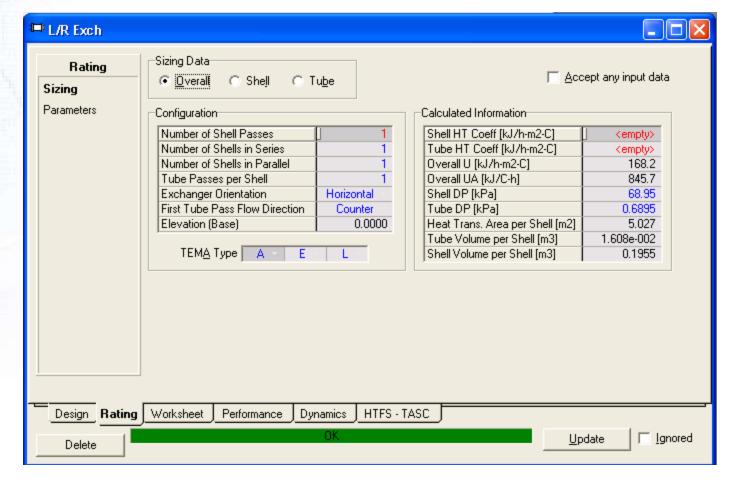


Unit Operation Interface (CAPE-OPEN)



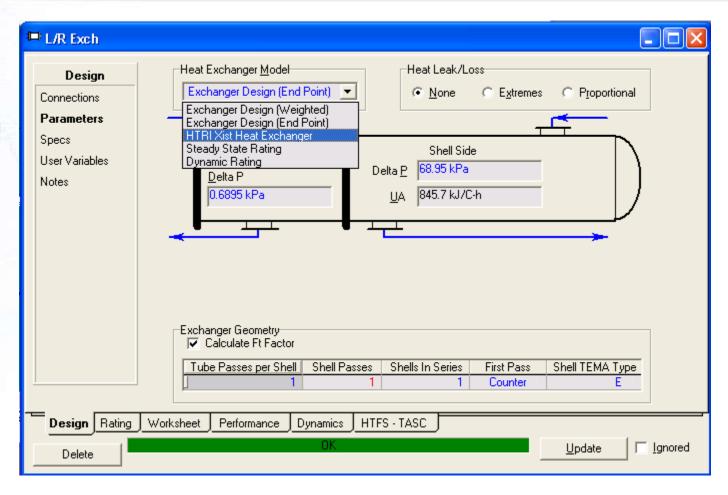


Unit Operation Interface (Native)





Unit Operation Interface (Extension)



Can CAPE-OPEN allow access to native unit operation interface?





 Unit Operation interface tested against HYSYS, ASPEN Plus, PRO/II, and UniSim Design

 Property package interface tested against ASPEN Plus, PPDS, Simulis, and UniSim Design





- Successful interface with one software package does not guarantee it will work with other packages
- Interface required modification for each new package tested
- Requires software packages to be available for testing and interaction between companies

Overall experience was successful in that common code used for all packages!





- Most problems have been related to properties
- For example overall enthalpy:
 - Software A: Calculated automatically via CalcFlash
 - Software B: Must be specified in the CalcFlash property list
 - Software C: Due to a bug CalcFlash throws an exception when property list supplied
 - Software D: Not calculated by CalcFlash, must be determined from phase properties
- Makes code more complex than necessary





- Examples of some other problems
 - Volume property calculated instead of Density.
 Modified HTRI software to detect this and use the available property.
 - IDispatch Invoke method not supported. Modified HTRI software to never use Invoke.
 - IPersistStorage interface not supported. Other vendors implemented IPersistStorage.





- Improved documentation
 - Flexibility interferes with standardization. Allowing both
 Volume or Density makes things more difficult not less
 - More specific mechanisms (e.g., overall enthalpy)
 - Required/recommended properties
- Better testing software





- Vendors could supply
 - Program specific testers
 - Allows testing of compatibility with particular software without requiring access to vendor software
 - Could be available to CAPE-OPEN members on website
 - Sample code
 - Provides additional examples beyond Mixer/Splitter block
 - Jump start for new members
- CAPE-OPEN could supply
 - Reference implementation
 - Would require multi-vendor support
 - Substantial amount of work





Summary and Conclusions

- Simply providing technically correct interfaces is not sufficient
- Vendors should optimize software for use in PME
- Additional work in PME could enhance adoption
- CAPE-OPEN could enhance documentation in some areas
 - Details of physical property handling
- Vendor specific testing tools/example code would be useful